

<u>BiOxySorb</u>: Economic low carbon power production and emissions control for future and flexible biomass co-fired power stations

Project Overview

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Economic low carbon power Production and Emissions Control for Future and Flexible Biomass Co-fired Power Stations

- 1. Introduction to the BiOxySorb Project
- 2. Background:
 - Oxy-fuel Combustion
 - Biomass Co-Combustion
 - Dry Sorbent Injection
- 3. BiOxySorb Work Packages & Combustion Test Facilities
- 4. BiOxySorb Publications
- 5. Summary



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BiOxySorb – Introduction

BiOxySorb:

Economic low carbon power production and emissions control for future and flexible biomass co-fired power stations

Project dates:

- Project start:
- Duration:
- End date:

01/07/2013

36+6 months

12/2016



BiOxySorb – Introduction

Strong consortium with industrial partners from all sectors affected by the investigated technologies:

• USTUTT (IFK): Academic research institute Germany -Public R&D institute • CIUDEN: Spain • Uniper: Utility UK • Lhoist: Producer of sorbents Belgium -**Boiler manufacturer** • GBS: Spain -



BiOxySorb – Introduction

Project objectives:

- Coal-fired power plants need to reduce carbon intensity:
 - Biomass co-combustion
 - Oxy-fuel combustion
 - Biomass co-combustion in oxy-fuel (negative C-balance!)
- New biomasses come into the market: 2nd generation biomass
- Flexible, low cost emission control required \rightarrow Dry sorbents
- How can systems be integrated and how do they perform?

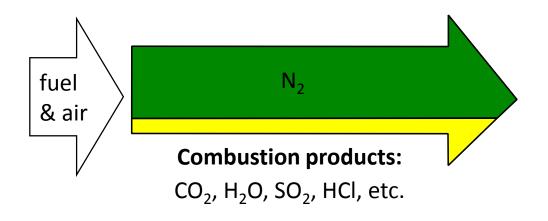


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Background: Air vs. Oxy-Fuel

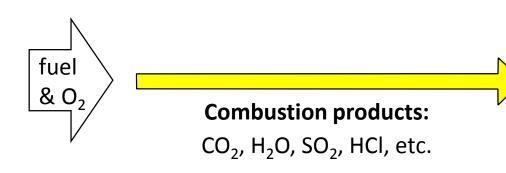
• <u>Air-fired</u> combustion:





Background: Air vs. Oxy-Fuel

<u>Oxy-fuel</u> combustion:



"Process-borne" impurities:

- CO, NO_x
- Little impacted by absence of N₂
- Concentration changes highly dependent on process conditions

Bioxy Sorb

Exclusion of airborne N₂:

Increase of acid gas

(when not removed)

•

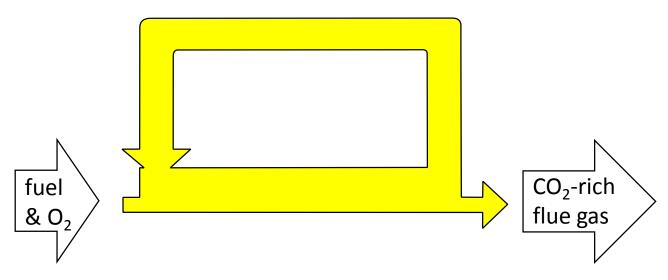
Generation of CO₂ rich gas for

sequestration/utilization

concentrations (factor 4-5)

Background: Air vs. Oxy-Fuel

• <u>Oxy-fuel</u> combustion:



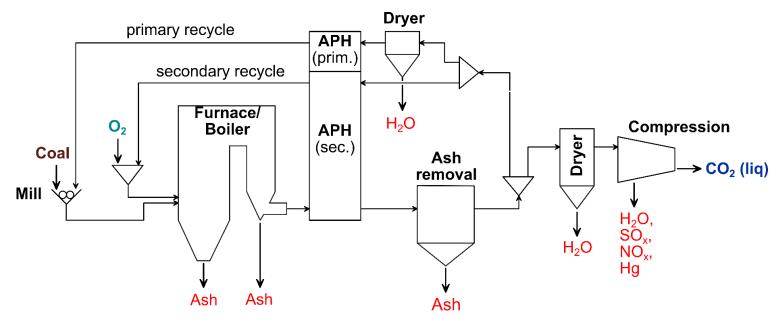
Flue gas recirculation to control:

- Temperatures
- Gas flows
- HEAT TRANSFER



Background: Oxy-Fuel Combustion

Practical oxy-fuel configuration for low S & Cl fuels



- Problems: E
- <u>s:</u> Excessive SO_x (& HCI) levels with most coals
 - SO_x (& HCI) control within recycle required to reduce corrosion
 - Final acid gas removal required before CO₂ liquefaction



Background: Oxy-Fuel Combustion

Oxy-fuel combustion: Status

- Feasibility proofed at pilot and demo scale (CIUDEN, Vattenfall, Callide Oxy-fuel Project)
- Most work focussed on mono-combustion of coal
- Limited experience/Knowledge gaps:
 - Biomass co-combustion in oxy-fuel conditions
 - Oxy-fuel combustion of 2nd generation biomasses
 - Fate of acid gases (SO_x, HCl) and trace elements (Hg)
 - Economic flue gas cleaning in oxy-fuel operation by DSI



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Background: Biomass Co-Combustion

• Biomass co-combustion: Status

- Widely applied in power plants; Most plants 5-15% co-firing
- Currently 1st generation biomasses
- Biomass co-combustion can be retrofitted
- Benefits of biomass as fuel:
 - Renewable energy source: <u>Carbon neutral</u>
 - "Clean" fuel: Lower harmful gas emissions (e.g. SO_x, Hg)

Co-combustion under in oxy-fuel plants:

- Lower SO_x, (HCl) and Hg levels in the boiler/flue gas
- <u>Negative carbon balance</u>





Background: Biomass Co-Combustion

- Second generation biomass: torrefied biomass
 - Lower moisture content & hydrophobic properties
 - Higher energy density and heating value
 - Easier storage and delivery
 - Easier milling in pulverized coal-fired plants
- <u>Limited experience/Knowledge gaps:</u>
 - Co-combustion of 2nd generation biomasses
 - Biomass co-combustion at high thermal shares
 - Milling/co-milling of 2nd generation biomasses
 - Emission behavior, ash qualities, slagging/fouling





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Background: Dry Sorbent Injection (DSI)

Acid gas (SO₂, SO₃, HCl) control by dry sorbents:

- Earth-alkali based: e.g. Ca(OH)₂, CaCO₃
 - $\succ Ca(OH)_2 + SO_2 \rightarrow CaSO_3 + H_2O$
 - > $Ca(OH)_2 + SO_2 + \frac{1}{2}O_2 \rightarrow CaSO_4 + H_2O$
 - \succ CaCO₃ + SO₂ + ¹/₂ O₂ → CaSO₄
- Alkaline based: e.g. NaHCO₃, Trona

Hg control by dry sorbents:

• Activated carbon, mineral based sorbents

Performance depends on:

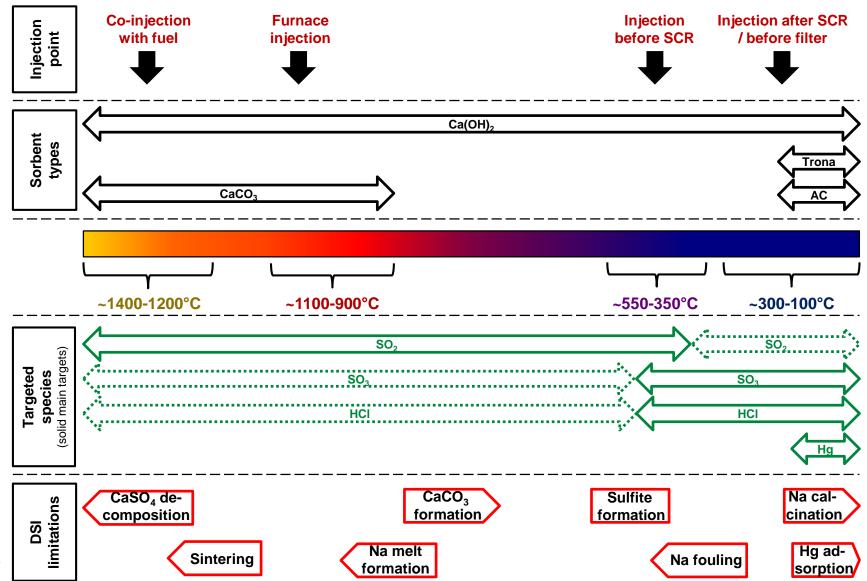
- **Sorbent reactivity** (e.g. porosity, active surface etc.)
- Process conditions (e.g. temperature, dispersion etc.)

(low temperature) (high temperature) (high temperature) (low temperature)

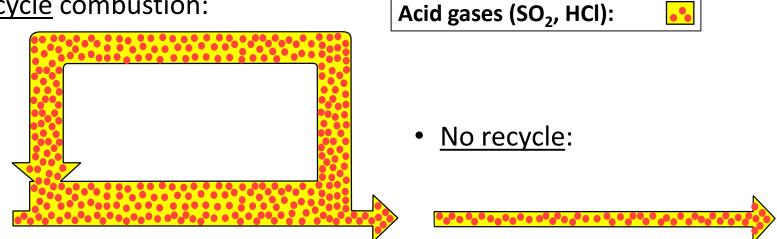
(low temperature)



Background: DSI in BiOxySorb

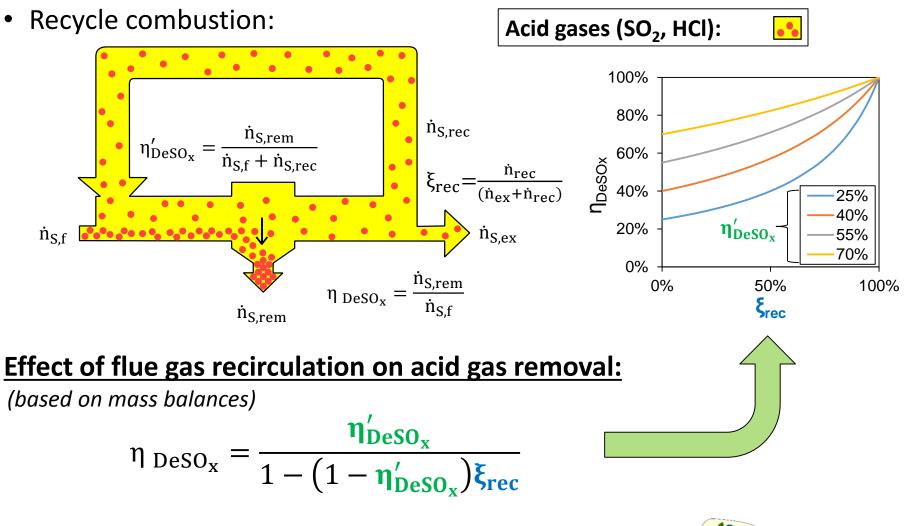


• <u>Recycle</u> combustion:

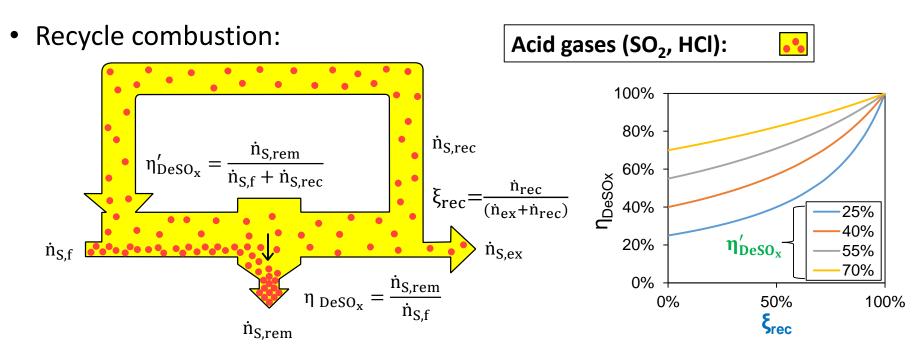


• Recycle combustion does not alter gas concentrations







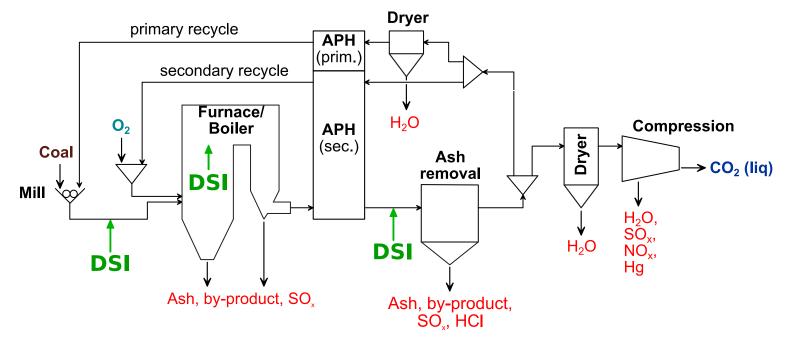


Effect of flue gas recirculation on acid gas removal:

- Practical residence time of impurities is extended (beneficial)
- Acid gas removal lowers initial impurity levels (negative)
- Both effects balance each other to some degree



Dry Sorbent Injection (DSI) [e.g. CaCO₃ or Ca(OH)₂]:



Benefits/drawbacks:

- + Low costs (no scrubber required)
- + No excessive gas cooling
- Dilution of ash



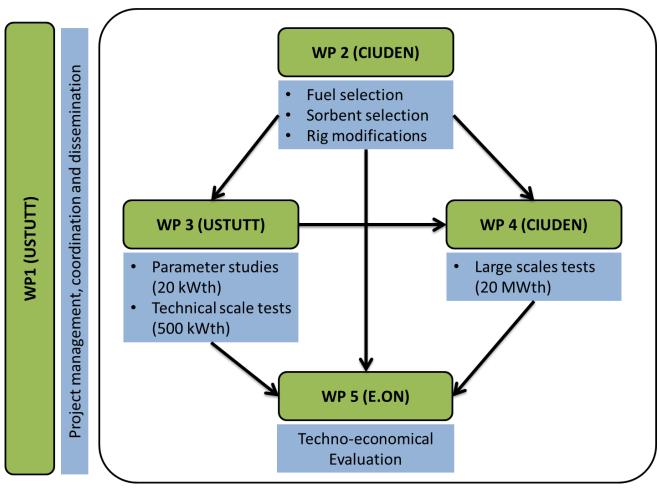
BiOxySorb – Dry Sorbent Injection

- Sorbents for SO_x, HCl and Hg control: Status
 - Widely applied for Hg control (USA)
 - Applied for acid gas removal (e.g. wood & MSW fired & FB systems)
 - Few applications for acid gas removal in coal/oil fired systems (USA, China)
- <u>Limited experience/Knowledge gaps:</u>
 - Potential of sorbents to increase flexibility of flue gas cleaning systems
 - Performance of sorbents under oxy-fuel condition
 - Integration of sorbent injection in oxy-fuel processes



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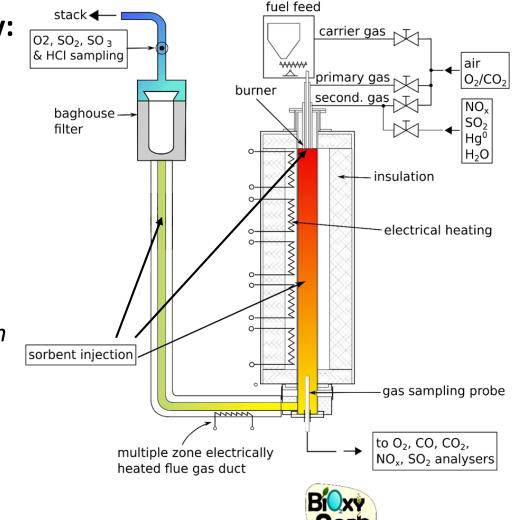




IFK's 20 kW el. heated facility:

- Air and simulated oxy-fuel operation
- Mono- and co-firing possible
- Very good accessibility for injection and sampling
- Highly flexible system

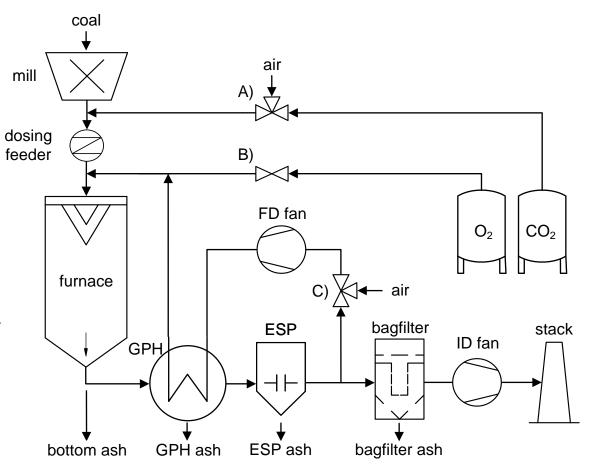
Used for WP3 <u>parametric studies</u> on co-combustion and DSI in air and oxy-fuel mode



IFK's 500 kW pilot rig:

- Air and oxy-fuel operation
- Mono- and co-firing
- Good accessibility for injection and sampling
- More realistic system
- 24 hour operation
- Less flexible & more costly

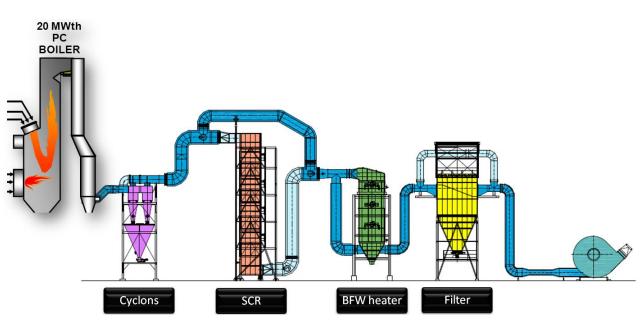
Used for WP3 <u>pilot studies</u> with selected co-combustion and DSI configurations in air and oxy-fuel mode





CIUDEN's 20 MW demo system:

- Ball mill (co-milling)
- Air and oxy-fuel operation
- Mono- and co-firing
- Good accessibility for injection and sampling
- Realistic: Industrial scale and outline
- 24 hour operation
- Less flexible & relatively costly



Used for WP4 <u>demonstration tests</u> with selected co-combustion and DSI configurations in air and oxy-fuel mode



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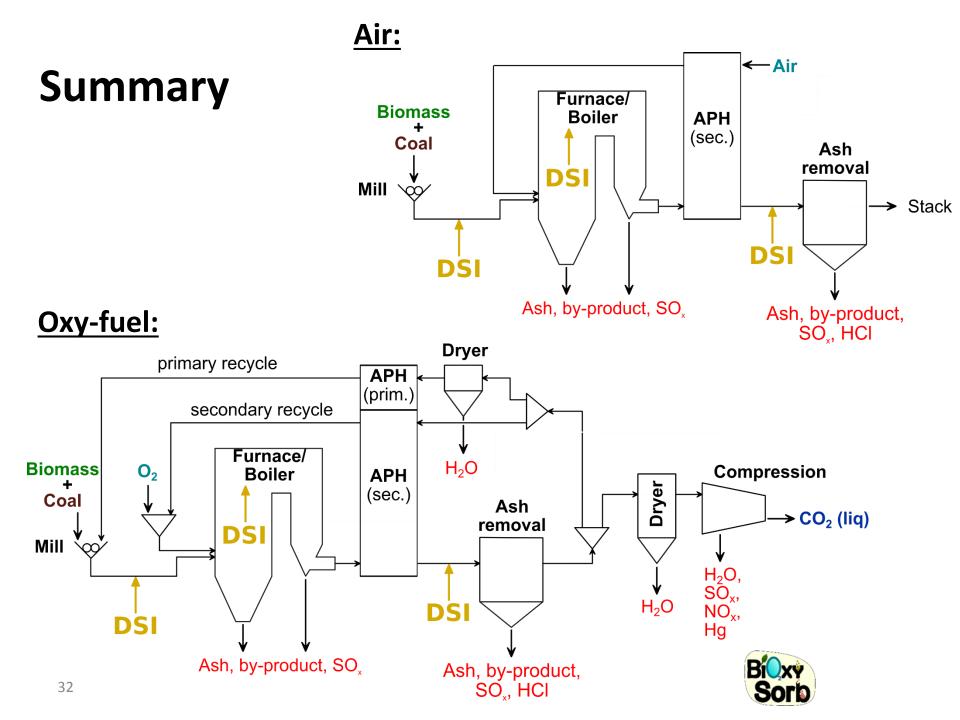
BiOxySorb: Publications

- <u>Poster:</u> **Presentation of the BiOxySorb Project**, *Reinhold Spörl et al. (IFK),* 3rd Oxyfuel Combustion Conference, 9th-13th September 2013, Ponferrada, Spain
- <u>Presentation:</u> Risk during co-firing oxy-mode, Miguel Angel Delgado et al. (CIUDEN), 4th IEA CCC Workshop on co-firing Biomass with Coal, 4-6th November 2014, Nittany Lion Inn, State College, Pennsylvania, USA.
- <u>Presentation:</u>
 The Impact of Co-combustion on Acid Gas and Mercury Emissions, Reinhold
 Qin et al. (IFK), 40th International Technical Conference on Clean Coal Fuel
 Systems 31st May-4th June 2015, Sheraton Hotel, Clearwater, Florida, USA.
- <u>Presentation:</u> Impact of Co-combustion and Oxy-Fuel Combustion on Flue gas Impurities, *Reinhold Spörl et al. (IFK)*, 5th Oxyfuel Combustion Research Network Meeting, 27th-30th October 2015, Wuhan, China
- <u>Presentation:</u> Acid Gas Control by Dry Sorbent Injection in Air and Oxy-Fuel Combustion, *Reinhold Spörl et al. (IFK)*, 5th Oxyfuel Combustion Research Network Meeting 27th-30th October 2015, Wuhan, China
- <u>Presentation:</u>
 Acid Gas Control by Dry Sorbent Injection in Air and Oxy-Fuel Combustion, *Reinhold Spörl et al. (IFK)*, 33rd Annual International Pittsburgh Coal Conference 8th-12th August 2016, Cape Town, South Africa.



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Thank you for your attention!

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